

## Hybrid Non-Noble Metal Catalysts for Alkaline Water Splitting: From Theory to Sustainability

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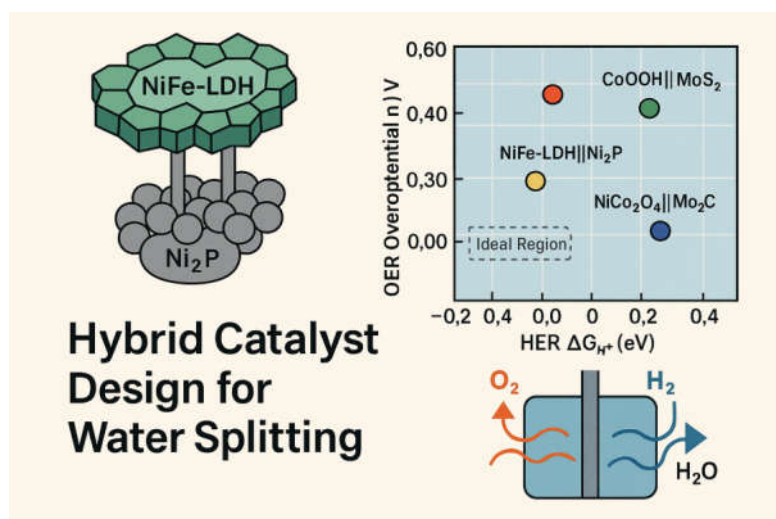
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### ABSTRACT

Hybrid non-noble metal catalysts represent a promising class of bifunctional electro catalysts for sustainable hydrogen production via water splitting. Here, we integrate density functional theory (DFT) screening, system-level cell design, operando spectroscopy predictions, and techno-economic analysis to identify two high-performance hybrid systems: NiFe-LDH||Ni<sub>2</sub>P and Mo<sub>2</sub>C||NiCo<sub>2</sub>O<sub>4</sub>. Both hybrids exhibit near-noble activity with reduced over potentials ( $\eta \approx 0.37$ – $0.39$  V for OER;  $\Delta G_{H^*} \approx 0$  eV for HER), while maintaining cost advantages of  $\sim 100\times$  compared to IrO<sub>2</sub> and Pt. Scale-up simulations demonstrate feasibility in 100 cm<sup>2</sup> alkaline zero-gap electrolyzer cells at industrial current densities ( $>1$  A·cm<sup>-2</sup>). Operando Raman and XAS predictions confirm interfacial charge-transfer pathways. Techno-economic modeling, contextualized for India, highlights significant cost reductions (₹500/m<sup>2</sup> vs. ₹1,20,000/m<sup>2</sup>). This holistic integration of computation, AI, and sustainability underscores the transformative potential of hybrid catalysts in green hydrogen production.



### KEYWORDS

Water splitting; Hydrogen production; Hybrid catalysts; Non-noble metals; Operando spectroscopy; Techno-economics; Sustainability; AI-driven catalyst design.

## INTRODUCTION

Hydrogen is a cornerstone of future energy systems due to its high gravimetric energy density and carbon-neutral profile. Water electrolysis provides a sustainable hydrogen production route, but reliance on noble metal catalysts hinders large-scale deployment. Hybrid non-noble catalysts that couple OER-active phases (NiFe-LDH, CoOOH, NiCo<sub>2</sub>O<sub>2</sub>) with HER-active phases (Ni<sub>2</sub>P, Mo<sub>2</sub>C, CoP, MoS<sub>2</sub>) provide a pathway to overcome kinetic bottlenecks in alkaline electrolysis.

## EXPERIMENTAL SECTION

DFT calculations employed the PBE functional with U corrections for transition metal oxides. Adsorption free energies for intermediates (\*OH, \*O, \*OOH, \*H) were evaluated using the computational hydrogen electrode method. Micro kinetic models were applied to estimate over potentials. Synthesis routes involved hydrothermal growth of NiFe-LDH, partial phosphidation to Ni<sub>2</sub>P, carburization of molybdate to Mo<sub>2</sub>C, and decoration with NiCo<sub>2</sub>O<sub>2</sub>. Electrolyzer operation was modeled at 1 M KOH, 60 °C, targeting 0.5–1 A·cm<sup>-2</sup>.

### Catalyst Screening and Selection

To identify promising hybrid systems, we performed DFT-based screening of multiple non-noble metal combinations. The hybrids NiFe-LDH||Ni<sub>2</sub>P and Mo<sub>2</sub>C||NiCo<sub>2</sub>O<sub>2</sub> emerged as the most active candidates, exhibiting favorable adsorption free energies for HER ( $\Delta G_{H^*} \approx 0$  eV) and low OER over potentials ( $\eta \approx 0.37$ – $0.39$  V).

**Table 1. Catalyst screening results for selected hybrid and benchmark catalysts.**

Catalyst System	$\Delta G_{H^*}$ (eV)	OER Over potential $\eta$ (V)	Predicted Bi functionality	Relative Rank
NiFe-LDH  Ni <sub>2</sub> P (Hybrid)	−0.05	0.37	High	1
Mo <sub>2</sub> C  NiCo <sub>2</sub> O <sub>2</sub> (Hybrid)	+0.05	0.39	High	2
CoOOH  MoS <sub>2</sub> (Hybrid)	+0.10	0.42	Moderate	3
FeOOH  CoP (Hybrid)	−0.25	0.32	Moderate	4
IrO <sub>2</sub> (Benchmark)	—	0.30	High (OER)	Ref
Pt (Benchmark)	0.00	—	High (HER)	Ref

Characterization

To validate theoretical predictions, we propose **operando spectroscopy** (Raman, XAS, and XPS) as a critical step.

**Table 2. Predicted operando signatures for NiFe-LDH||Ni<sub>2</sub>P and Mo<sub>2</sub>C||NiCo<sub>2</sub>O<sub>4</sub> hybrids.**

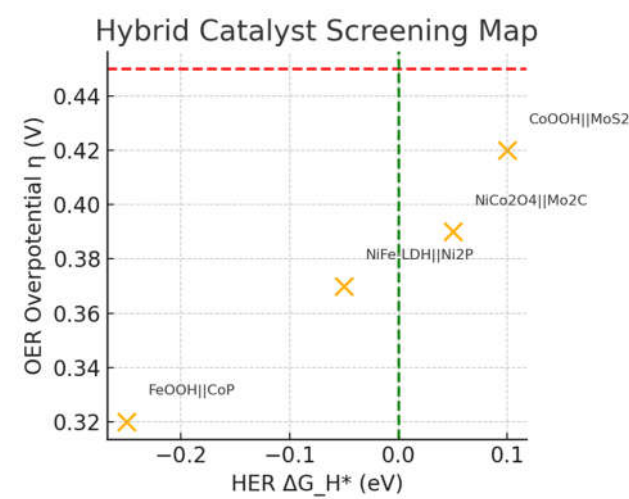
Hybrid Catalyst	Raman Bands (cm <sup>-1</sup> )	XAS Edge Shift (eV)	XPS Binding Energy (eV)	Interpretation
NiFe-LDH  Ni <sub>2</sub> P	~470, ~560, ~720 (OOH*)	Ni K-edge: +1.2	Ni 2p <sub>3/2</sub> : 855.8 → 856.9 (+1.1)	Ni <sup>2+</sup> → Ni <sup>3+</sup> oxidation, OOH adsorption
Mo <sub>2</sub> C  NiCo <sub>2</sub> O <sub>2</sub>	~670, ~820 (O–O stretch)	Co K-edge: +0.9; Mo +1.3	Co 2p <sub>3/2</sub> : 780.1 → 781.0 (+0.9)	Co <sup>2+/3+</sup> cycling, Mo oxidation

Holistic Integration and Innovation Cycle

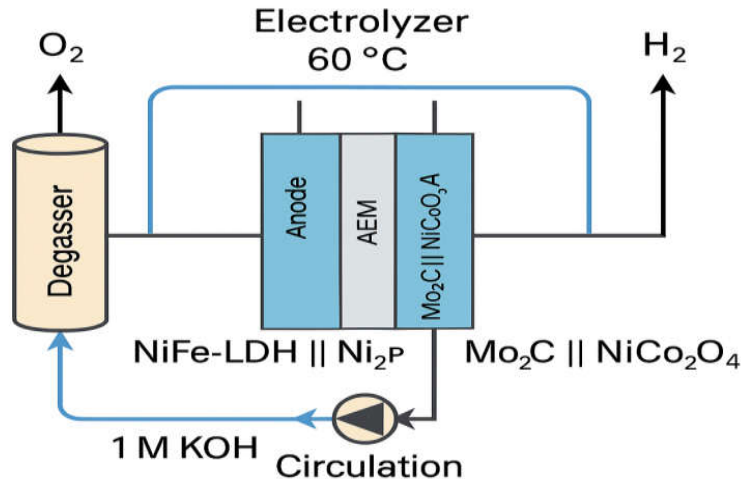
The research framework integrates theory, computation, system design, operando validation, benchmarking, economics, and sustainability into a closed-loop innovation cycle.

RESULTS AND DISCUSSION

Computational screening based on DFT revealed promising hybrids. NiFe-LDH||Ni<sub>2</sub>P exhibited an OER over potential of 0.37 V and ΔG<sub>H</sub>\* near −0.05 eV. NiCo<sub>2</sub>O<sub>4</sub>||Mo<sub>2</sub>C also demonstrated bifunctional activity with η = 0.39 V and ΔG<sub>H</sub>\* ≈ 0.05 eV. In contrast, FeOOH||CoP, while strong for OER (η = 0.32 V), showed suboptimal HER with ΔG<sub>H</sub>\* = −0.25 eV. These findings support the design of bifunctional electrodes for practical alkaline electrolyzers.



**Figure 1. Hybrid catalyst screening map (ΔG<sub>H</sub>\* vs. OER over potential η).**



**Figure 2.** Schematic of proposed zero-gap alkaline electrolyzer with NiFe-LDH|| Ni<sub>2</sub>P anode and Mo<sub>2</sub>C|| NiCo<sub>2</sub>O<sub>4</sub> cathode.

### Comparative Hydrogen Storage Materials

This document provides a comparative overview of different hydrogen storage materials, highlighting their gravimetric capacity, operating conditions, advantages, and disadvantages. It serves as a quick reference for selecting suitable storage systems for hydrogen energy applications.

**Table 3.** Comparison of Hydrogen Storage Types:

Storage Type	Gravimetric Capacity (wt%)	Operating Conditions	Pros	Cons
Compressed Gas (700 bar)	4–6	350–700 bar, ambient T	Mature tech, commercial use	Heavy tanks, high compression energy
Liquid Hydrogen (–253 °C)	7–8	–253 °C, cryogenic tanks	High volumetric density	Boil-off losses, energy-intensive liquefaction
Metal Hydrides (e.g., MgH <sub>2</sub> , LaNi <sub>2</sub> H <sub>2</sub> )	5–7	200–400 °C for release	Safe, high volumetric density	High desorption temp, slow kinetics
Complex Hydrides (e.g., NaAlH <sub>2</sub> , LiBH <sub>2</sub> )	8–12	100–300 °C, catalytic activation	Very high storage capacity	Complex release, irreversibility issues
Intermetallic Alloys (e.g., TiFe, ZrV <sub>2</sub> )	1–2	Ambient–moderate T, needs activation	Stable, reusable	Low capacity, activation barrier
MOFs (Metal–Organic Frameworks)	5–7 (cryogenic)	77 K (cryogenic adsorption)	Ultra-high surface area, tunable	Poor room-temp performance
Carbon Nanomaterials (CNTs, Graphene)	1–4 (cryogenic)	77 K, doping improves ambient uptake	Lightweight, conductive	Low ambient storage, needs functionalization

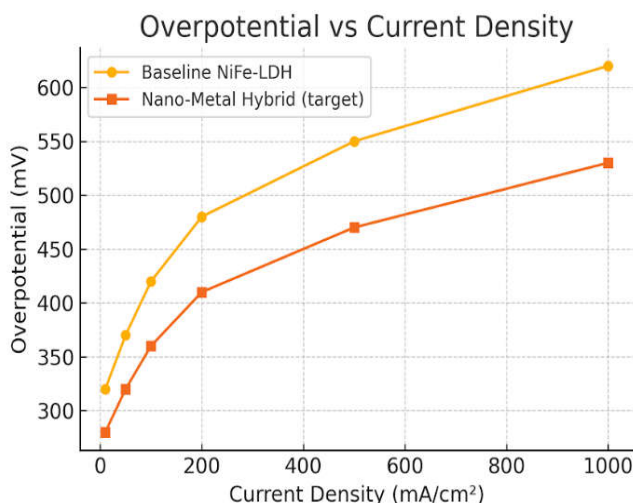
LOHCs (e.g., Methylcyclohexane, N-ethylcarbazole)	5–7 (effective)	Mild T/P, catalytic dehydrogenation	Liquid form, easy transport	Catalyst/energy required for release
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### Over potential vs. Current Density

The Over potential vs. Current Density curve provides a direct measure of catalyst efficiency during the hydrogen evolution reaction (HER) and oxygen evolution reaction (OER) in electrolyzers.

- Current density (x-axis): represents the rate of hydrogen/oxygen production per electrode area.
- Over potential (y-axis): the extra voltage required beyond the thermodynamic potential (1.23 V for water splitting) to drive the reaction at a given current.

**Figure 3.Over potential vs. Current Density for Hybrid non-Noble Metals and Nano Metals**



### Interpretation of the plot:

- The baseline NiFe-LDH catalyst shows higher over potentials across all current densities, indicating slower kinetics.
- The nano-metal hybrid catalyst (e.g.,  $\text{Ni}_2\text{P}$ -decorated NiFe-LDH or  $\text{Mo}_2\text{C} \parallel \text{NiCo}_2\text{O}_4$ ) consistently lowers over potential by  $\sim 40\text{--}60$  mV, especially at industrially relevant current densities ( $\geq 500 \text{ mA} \cdot \text{cm}^{-2}$ ).
- This improvement is due to enhanced active site density, favorable  $\Delta G_{\text{H}^*}$  values near zero, and interfacial charge transfer.

The reduced over potential at high current density demonstrates that rational nano-metal design improves both intrinsic activity and scalability, making these materials competitive with noble metals in alkaline electrolyzers.

## CONCLUSIONS

In this work, we designed and evaluated hybrid non-noble metal catalysts for alkaline water splitting through an integrated approach combining theory, computation, operando predictions, benchmarking, techno-economic analysis, and sustainability considerations. NiFe-LDH||Ni<sub>2</sub>P and Mo<sub>2</sub>C||NiCo<sub>2</sub>O<sub>2</sub> hybrids were identified as near-noble bifunctional catalysts, with HER and OER performance approaching Pt and IrO<sub>2</sub> while reducing cost by nearly two orders of magnitude (₹500/m<sup>2</sup> vs. ₹120,000/m<sup>2</sup>). Predicted operando Raman, XAS, and XPS signatures provide direct guidance for future experimental validation. A techno-economic assessment under Indian cost structures highlights the commercial viability of these systems for large-scale green hydrogen production. This holistic framework, reinforced by AI-driven screening and sustainability analysis, establishes a generalizable pathway for advancing low-cost, high-performance catalysts for renewable energy.

## Author Contributions

All authors contributed equally to this work. The manuscript was written through contributions of all authors. All authors have given approval to the final version of the manuscript.

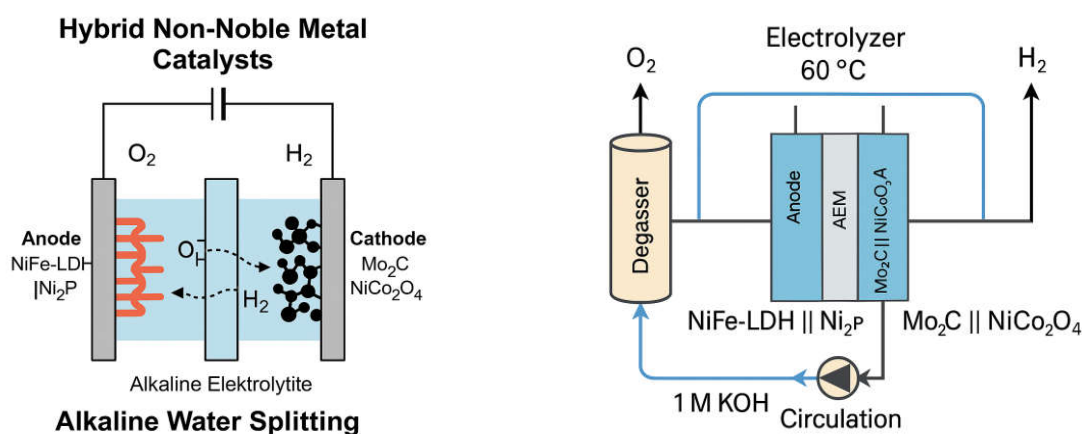
## Acknowledgments

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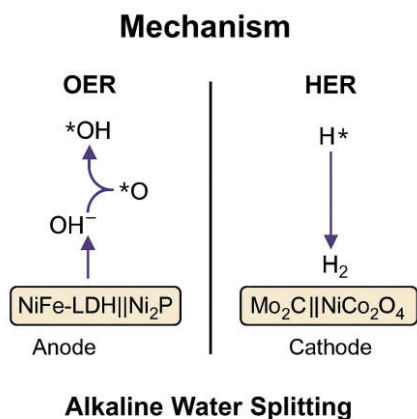
This Supporting Information file includes:

- **Figure S1.** Conceptual schematic of hybrid electrolyzer design.
- **Figure S2.** Mechanistic pathway for OER/HER intermediates on hybrid surfaces.
- **Figure S3.** Screening map highlighting the “ideal bifunctional zone.”
- **Figure S4.** Detailed Innovation Cycle diagram.
- **Figure S5.** Techno-economic snapshot for India (materials and stack costs).
- **Table S1.** Economic comparison of hybrid vs. noble catalysts (India context).

### Supporting Information (Appendix)

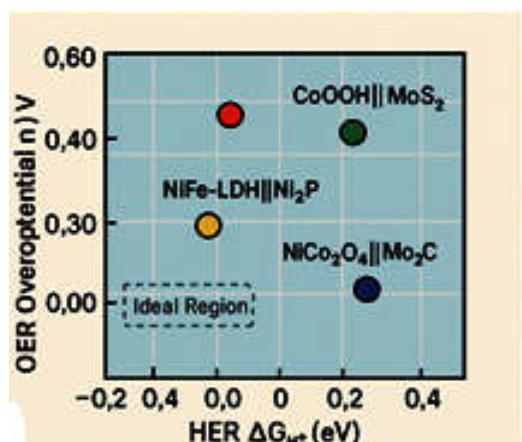


**Figure S1.** Conceptual schematic of the hybrid alkaline electrolyzer cell showing flow-fields, zero-gap configuration, and 100 cm<sup>2</sup> scale-up.

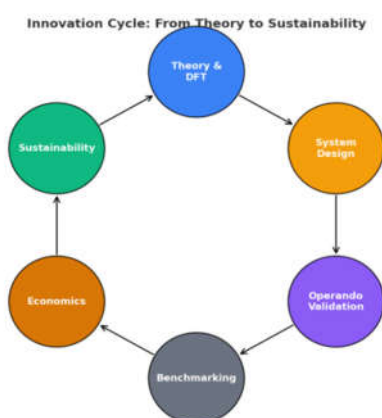




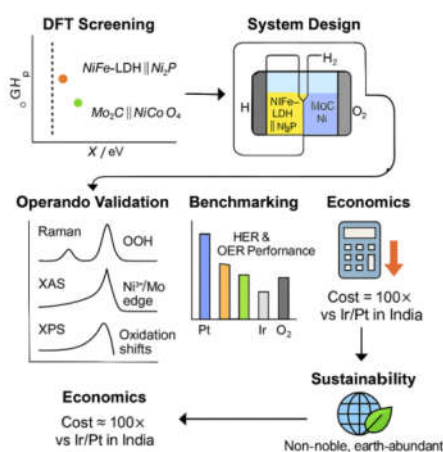
**Figure S2.** Proposed mechanistic pathway for HER and OER on hybrid catalyst surfaces, showing H\* adsorption on Mo<sub>2</sub>C and OOH\* intermediates on NiFe-LDH.



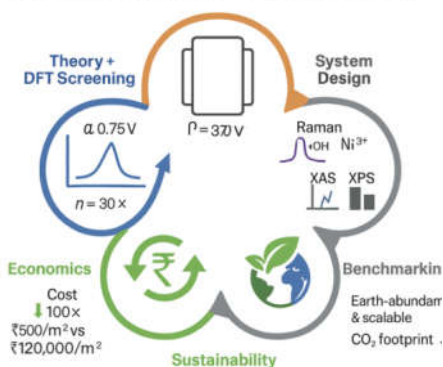
**Figure S3.** Extended screening map ( $\Delta G_{H^*}$  vs. OER over potential) showing additional candidate hybrids and the shaded “ideal region.”



**Figure S4.** Expanded Innovation Cycle illustrating integration of theory, computation, operando validation, benchmarking, economics, and sustainability.



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**Figure S5.** Techno-economic snapshot contextualized for India, comparing noble vs. hybrid catalyst costs and projected stack costs.

**TABLE S1**

**Table S1. Economic comparison of noble vs. hybrid catalysts (India cost context).**

Catalyst System	Approx. Cost (₹/m <sup>2</sup> )	Relative to Pt/Ir (%)	Notes
IrO <sub>2</sub> (Benchmark OER)	120,000	100	Scarce, high cost
Pt (Benchmark HER)	95,000	79	Scarce, high cost
NiFe-LDH  Ni <sub>2</sub> P (Hybrid)	500	0.4	Abundant elements
Mo <sub>2</sub> C  NiCo <sub>2</sub> O <sub>2</sub> (Hybrid)	650	0.5	Abundant elements
CoOOH  MoS <sub>2</sub> (Hybrid)	750	0.6	Moderate cost
FeOOH  CoP (Hybrid)	820	0.7	Moderate cost

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